



Benefits of Multi-Pollutant Catalyst Technology for Combustion Turbine Power Plants

Chris Bertole, Ph.D.

Cormetech, Inc.

VGB WORKSHOP "FLUE GAS CLEANING 2016"

Cormetech, Inc.



SCR catalyst design, manufacturing and testing:

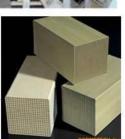
Coal Gas Diesel Fuel Oil

Stationary Power Refinery & Process Marine



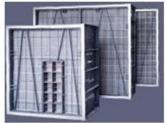
CORMETECH

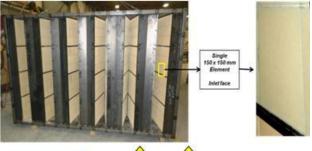
Hg Oxidation Catalyst

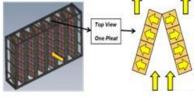






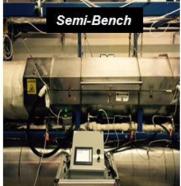














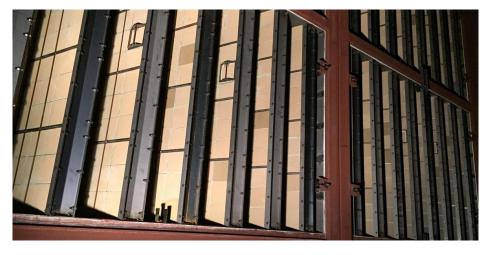


Presentation Overview



■ Multi-Pollutant Catalyst (METEOR™)

- > Concept
- Data and Validation
- ➤ Full-Scale Installation

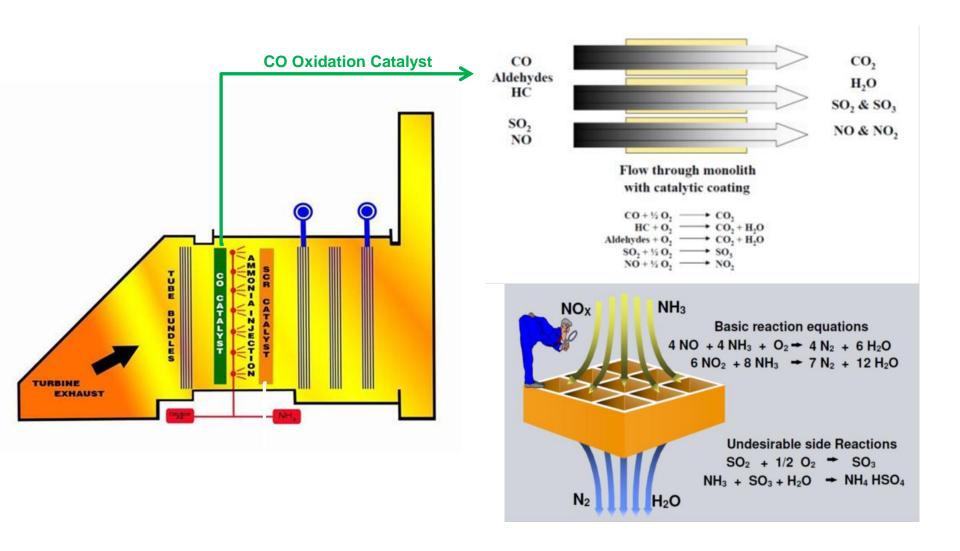






Traditional HRSG Catalyst Layout



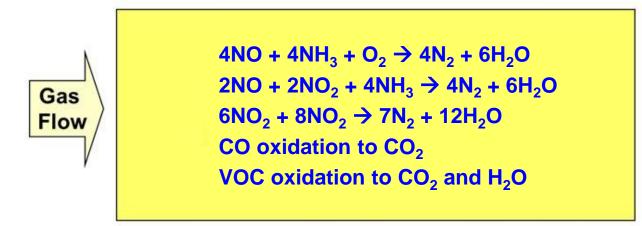


Multi-Pollutant Catalyst: METEORTM



- Homogeneously extruded honeycomb catalyst (1 layer)
- SCR functionality → V₂O₅-WO₃/TiO₂
- Oxidation functionality → PGM (Pd and/or Pt)
- Initially developed and patented by Siemens Energy (US 7,390,471)
- Optimized and fully developed into commercial production by Cormetech

Compounds Removed



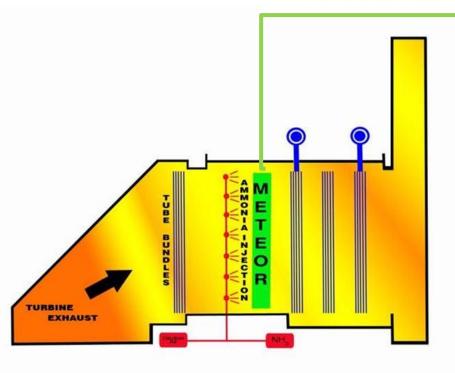


Installed in the place of traditional SCR

New HRSG Catalyst Layout







Oxidizing Function:

CO oxidation to CO₂
VOC oxidation to CO₂ and H₂O

Reduction Function:

 $4NO + 4NH_3 + O_2 \rightarrow 4N_2 + 6H_2O$

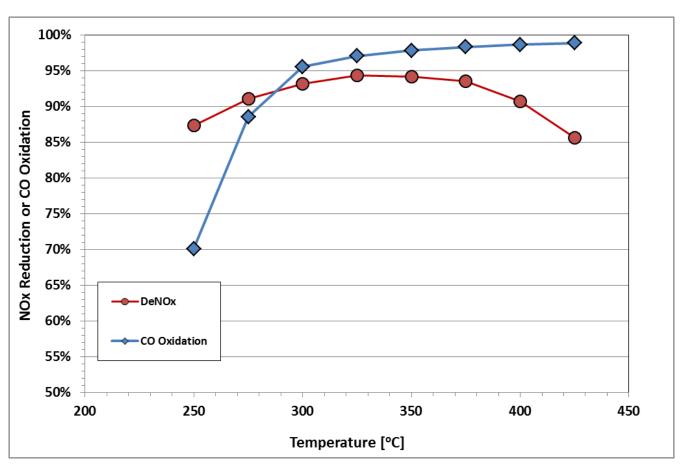
 $2NO + 2NO_2 + 4NH_3 \rightarrow 4N_2 + 6H_2O$

 $6NO_2 + 8NO_2 \rightarrow 7N_2 + 12H_2O$





- DeNOx and CO oxidation → high conversion rates over wide temperature range.
- PGM loading can be adjusted to optimize performance at low/high temperature.



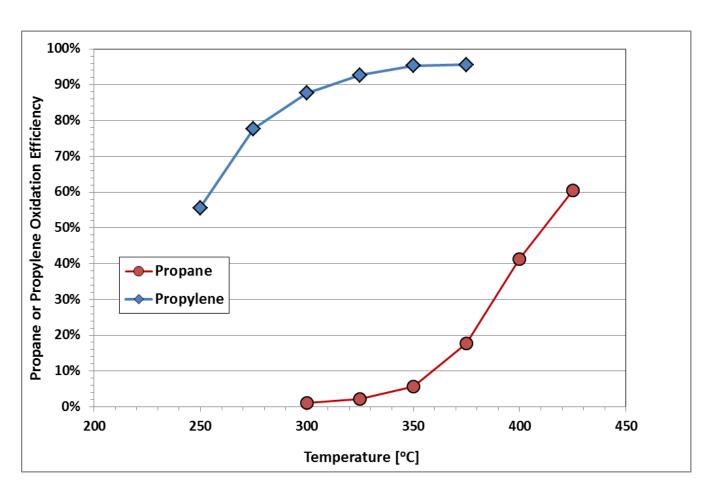
Test Conditions

NOx = 25 ppm CO = 25 ppm O_2 = 15% H_2O = 7% NH₃ slip 3 - 7 ppm Constant SV





Active for VOC oxidation \rightarrow rate depends on hydrocarbon speciation.



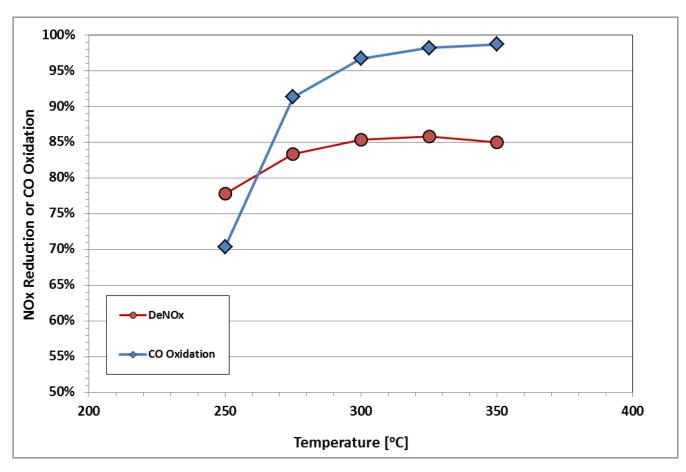
Test Conditions NOx = 25 ppm

 $O_2 = 15\%$ $H_2O = 7\%$ $[C_3H_8 = 20 \text{ ppm, or } C_3H_6 = 20 \text{ ppm]}$ $NH_3 \text{ slip } 3 - 7 \text{ ppm}$ Constant SV





- Effective DeNOx and CO oxidation for high inlet NOx & CO concentration cases.
- PGM loading can be adjusted to optimize performance at low/high temperature.



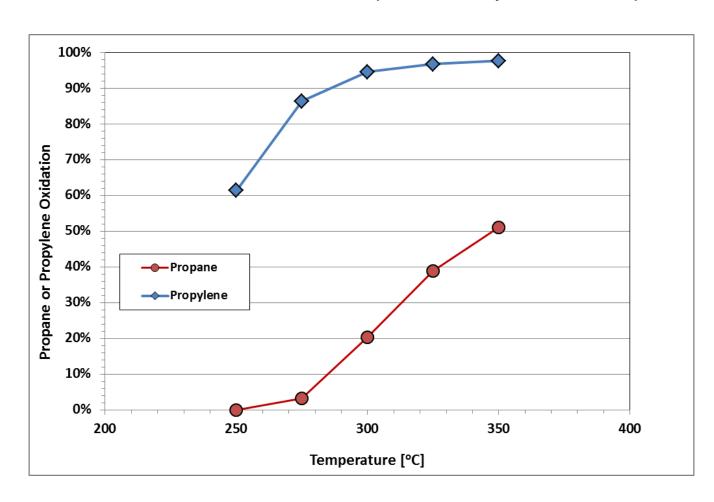
Test Conditions

NOx = 1000 ppm CO = 1000 ppm $O_2 = 8\%$ $H_2O = 8\%$ $C_3H_8 = 50 ppm$ $C_3H_6 = 50 ppm$ $NH_3/NOx = 0.91$ Constant SV





Active for VOC oxidation → rate depends on hydrocarbon speciation.



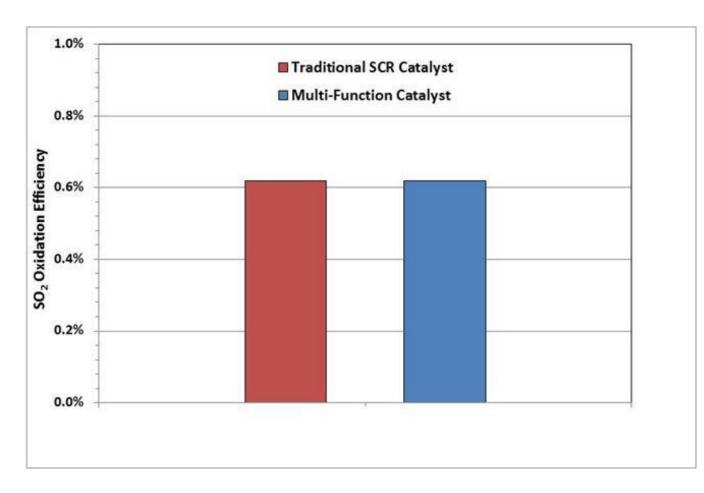
Test <u>Conditions</u> NOx = 1000 ppm CO = 1000 ppm $O_2 = 8\%$

 $H_2^2O = 8\%$ $C_3H_8 = 50 \text{ ppm}$ $C_3H_6 = 50 \text{ ppm}$ $NH_3/NOx = 0.91$ Constant SV





Similar SO₂ oxidation rate as traditional SCR catalyst.



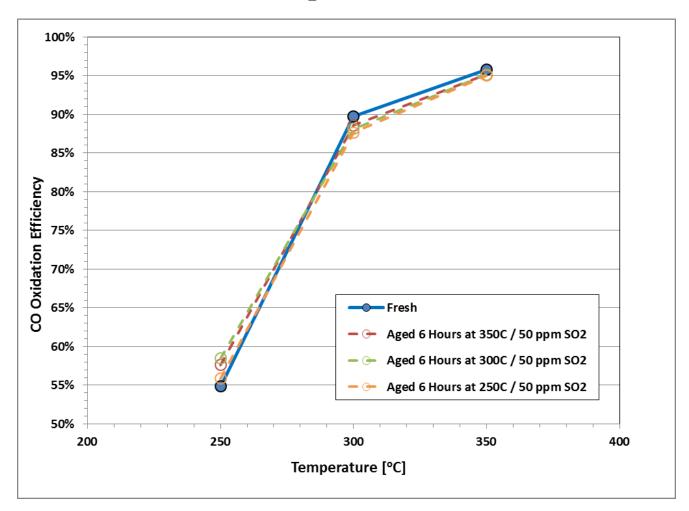
Test Conditions

 $T = 350^{\circ}\text{C}$ NOx = 35 ppm Inlet MR = 1.1 $O_2 = 15\%$ $H_2O = 8\%$ CO = 100 ppm $SO_2 = 500 \text{ ppm}$ Constant SV

SO₂ Durability



Short-term exposure to **50 ppm SO₂** has **no significant impact** on CO oxidation.



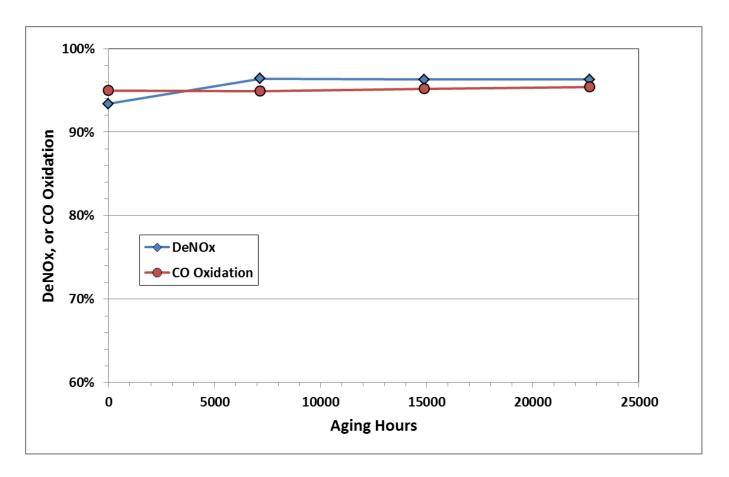
Test Conditions

 $\begin{aligned} &\text{NOx} = 25 \text{ ppm} \\ &\text{Inlet MR} = 1.1 \\ &\text{O}_2 = 15\% \\ &\text{H}_2\text{O} = 5\% \\ &\text{CO} = 100 \text{ ppm} \\ &\text{Constant SV} \end{aligned}$

Long Term Durability Field Test



- Full size element was installed in an existing SCR catalyst layer within a HRSG.
- Performance was periodically assessed → good durability after 22,660 hours.



METEORTM Benefits Summary



- Simplicity: one catalyst layer vs. two.
 - Smaller footprint in HRSG.
 - Lower pressure drop.
 - Lower O&M costs.
- Flexibility: applicable to new units, retrofits, and replacements.
- Lower SO₂ oxidation rate, relative to the traditional two catalyst layout.
 - Potential for reduced backend fouling.
- Highly resistant to sulfur compounds in the flue gas.

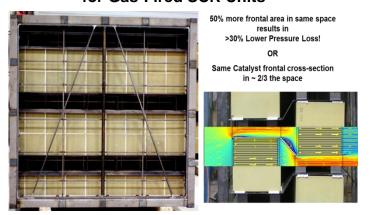
Module Options for Lower DP



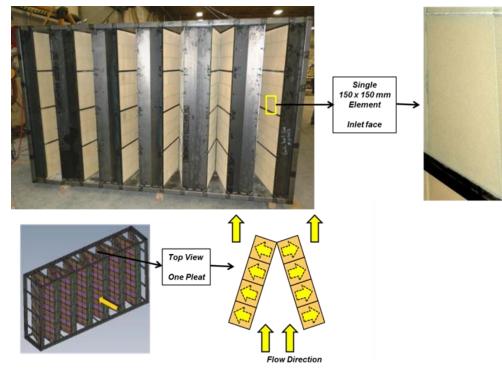
Traditional Horizontal Flow "Standard Module"



Patented "Advanced Module" for Gas-Fired SCR Units



Patent Pending "Elite™" Ultra-High Surface Area Module for Deeper Reduction in Pressure Drop for Gas-Fired SCR Units





- Plant location = Texas.
- Westinghouse 501G unit combustion turbine (~300MW electrical generation).
- METEOR™ fully replaced the existing SCR catalyst layer in November 2015.
- Guaranteed emission reductions of NOx, NH₃ slip, CO and VOC.
- Successful unit startup. Greater operating load flexibility during off-peak hours.



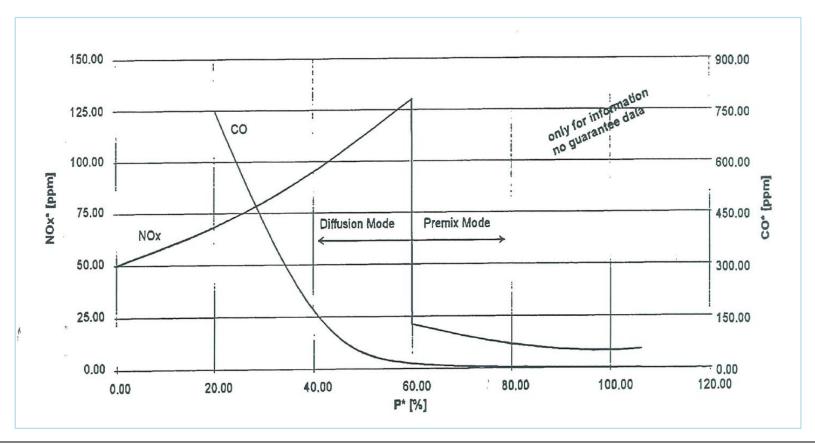
Increased CO Emissions at Low GT Load





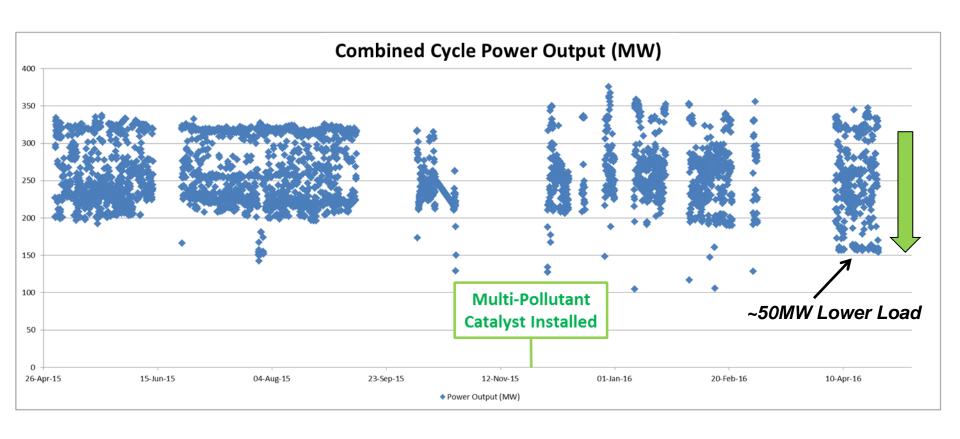
Replacement of existing SCR layer with a new METEOR™ catalyst layer enabled:

- (1) Capability to operate at lower loads while maintaining CO emission compliance.
- (2) Faster compliance of CO emissions during unit startup.



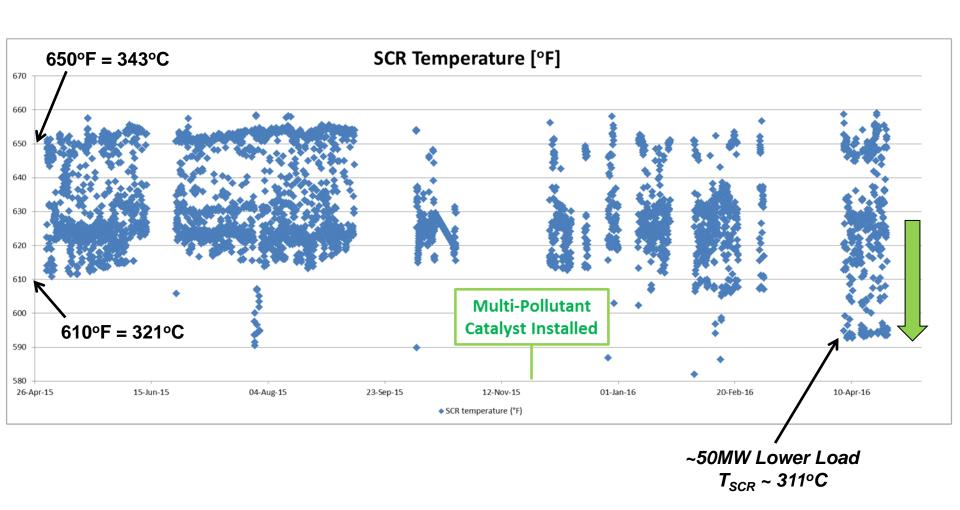
Increased Unit Turndown Capability = ~50MW





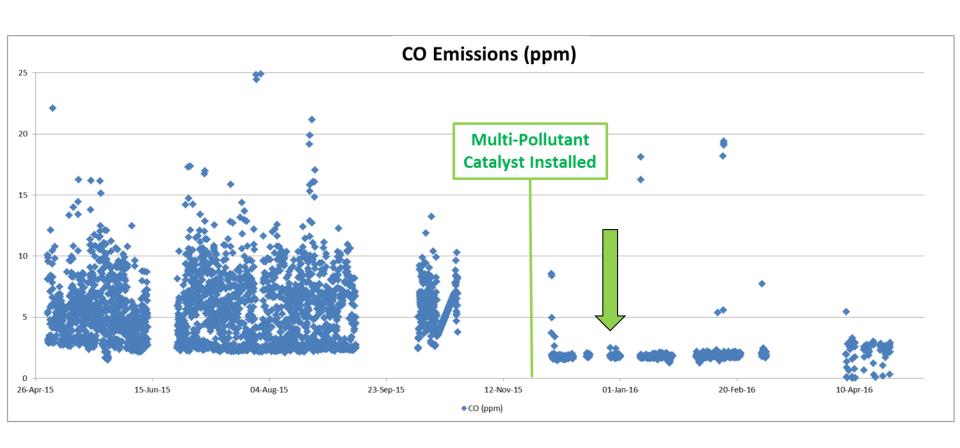
Lowest SCR Temperatures Decreased by ~10°C





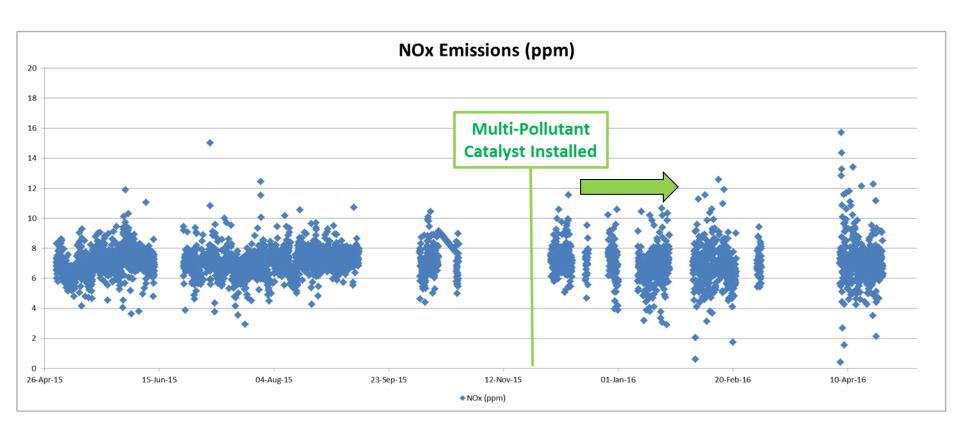






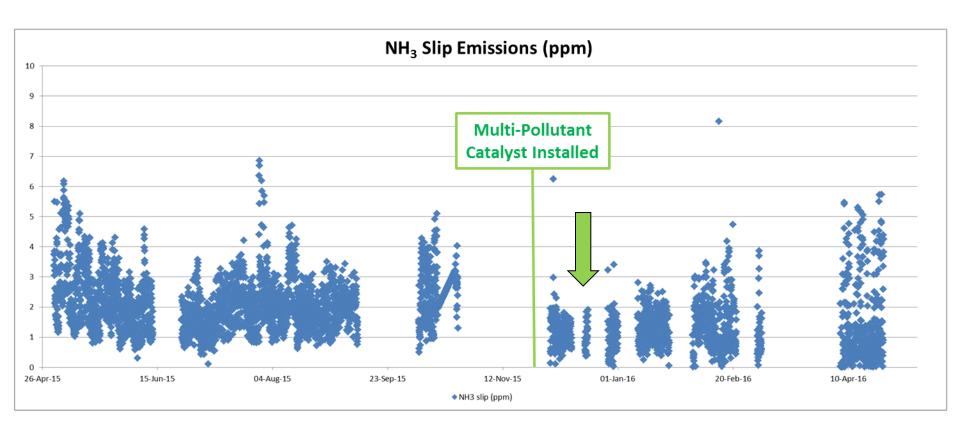
Same NOx Emissions (Per Design)











Field Test Validation



- Plant's motivation for METEOR™ installation:
 - Greater operating load flexibility during off-peak hours.
- Field testing validation: measured SCR inlet and outlet gas composition
 - SCR inlet = GT exhaust gas.
 - > Fresh catalyst achieved ~99% CO oxidation at 36% GT load point.
 - ➤ DeNOx achieving target value. NH₃ slip is very low due to the fresh catalyst state.

	GT Exhaust Gas Composition			SCR Outlet Gas Composition		Meteor SCR Catalyst Performance		
GT Load	SCR Temperature (°C)	GT Exhaust CO (ppm)	GT Exhaust NOx (ppm)	SCR Outlet CO (ppm)	SCR Outlet NOx (ppm)	SCR CO Oxidation	SCR DeNOx	SCR Outlet NH ₃ Slip (ppm)
98%	342	0.5	29.4	0.0	7.8	100%	74%	0.7
76%	334	0.6	32.8	0.0	6.7	100%	80%	0.7
36%	322	172	44.0	2.2	6.7	98.8%	85%	0.5

Summary

METEOR™ Multi-Pollutant Catalyst



- Simultaneously reduces NOx, CO, VOCs and NH₃ slip to compliance levels in one catalyst layer located at the traditional SCR catalyst location.
 - Lower system pressure drop.
- Provides benefits:
 - Total emissions regulation compliance.
 - Extended operating flexibility by extending the unit load operating range.
 - Reduction of corrosion of the HRSG section downstream of the SCR.
 - Lower O&M costs.
- Applicable to new units, retrofits, and replacements.
- Has been successfully deployed at a full-scale combined cycle HRSG unit.

